

1 **The effect of the source of microorganisms on adaptation of hydrolytic consortia**  
2 **dedicated to anaerobic digestion of maize silage**

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18 **Keywords**

19 maize silage, hydrolytic bacteria, adaptation, anaerobic digestion

20 **Abstract**

21 The main aim of this study was to evaluate the effect of the source of microorganisms on the  
22 selection of hydrolytic consortia dedicated to anaerobic digestion of maize silage. The  
23 selection process was investigated based on the analysis of changes in the hydrolytic activity

24 and the diversity of microbial communities derived from (i) a hydrolyzer of a commercial  
25 agricultural biogas plant, (ii) cattle slurry and (iii) raw sewage sludge, during a series of 10  
26 passages. Following the selection process, the adapted consortia were thoroughly analyzed for  
27 their ability to utilize maize silage and augmentation of anaerobic digestion communities.

28         The results of selection of the consortia showed that every subsequent passage of each  
29 consortium leads to their adaptation to degradation of maize silage, which was manifested by  
30 the increased hydrolytic activity of the adapted consortia. Biodiversity analysis (based on the  
31 16S rDNA amplicon sequencing) confirmed the changes microbial community of each  
32 consortium, and showed that after the last (10th) passage all microbial communities were  
33 dominated by the representatives of *Lactobacillaceae*, *Prevotellaceae*, *Veillonellaceae*.

34 The results of the functional analyses showed that the adapted consortia improved the  
35 efficiency of maize silage degradation, as indicated by the increase in the concentration of  
36 glucose and volatile fatty acids (VFAs), as well as the soluble chemical oxygen demand  
37 (sCOD). Moreover, bioaugmentation of anaerobic digestion communities by the adapted  
38 hydrolytic consortia increased biogas yield by 10-29%, depending on the origin of the  
39 community. The obtained results also indicate that substrate input (not community origin) was  
40 the driving force responsible for the changes in the community structure of hydrolytic  
41 consortia dedicated to anaerobic digestion.

## 42 **1. Introduction**

43         Over the past decades the biogas production technology has been focused on the  
44 development and optimization of systems characterized by high rate of anaerobic digestion of  
45 energy crops and solid agro-industrial wastes [1]. The anaerobic digestion process consists of  
46 two phases. In the first one, the substrate is converted mainly to soluble organic compounds  
47 such as volatile fatty acids (VFAs), which are then used in the second phase by methanogens

48 to produce biogas [2]. These two phases can be carried out simultaneously in a single  
49 bioreactor or separately, in a two-step system, which consists of two connected bioreactors.  
50 Due to their simplicity, many full-scale biogas plants in Europe utilize single-step systems.  
51 However, two-step technologies may ensure optimal conditions for each of the processes,  
52 which is especially crucial, as hydrolysis of complex polysaccharides such as cellulose or  
53 lignocellulose is often the rate-limiting step of the entire biogas production process. The  
54 production of VFAs proceeds much faster than the conversion of VFAs to methane, thereby  
55 causing acid accumulation, often leading to a drop in pH below 6, and consequently, to the  
56 inhibition of methanogenesis [3].

57 Two-stage anaerobic digestion allows to overcome the problem of imbalance between  
58 the acidogenesis and methanogenesis processes. Moreover, the two-stage technology enables  
59 the separation of solid and liquid phases and thus maintaining of a high rate of biogas  
60 production. Therefore, the use of the two-stage systems may lead to a higher overall reaction  
61 rate and biogas yield, and for this reason they are considered more effective than the  
62 conventional single-step technologies [4,5]. Moreover, some authors reported that splitting  
63 and separate optimization of hydrolysis/acidogenesis and methanogenesis could enhance the  
64 overall reaction rate, maximize biogas yields, and make the process easier to control, both  
65 under mesophilic and thermophilic conditions [4,5].

66 One of the most important problems encountered at commercial agriculture biogas  
67 plants is the start-up of new anaerobic reactors. According to Ahring [6], without efficient  
68 hydrolytic microbial consortium, the start-up period of thermophilic anaerobic digestion can  
69 be prolonged to one year before it enters a steady state. Selection of microorganisms  
70 responsible for different stages of anaerobic digestion, from the initial inoculum may be very  
71 long when is carried out during the start-up of anaerobic bioreactors. This often generates  
72 high operating costs for biogas plants. Therefore, the search for efficient consortia sources,

73 their selection and adaptation, as well as the choice of the main substrate, are the most  
74 important factors affecting the successful start-up of anaerobic digestion.  
75 The substrate used for anaerobic digestion is vary between the biogas production plants.  
76 Maize silage is one of the most popular energy crops and is widely used in agricultural biogas  
77 facilities as a substrate for the biogas production, and it represents 73% mass of the plant  
78 biomass processed in the biogas plants [7]. To increase biogas production from maize silage,  
79 various methods can be used, including chemical, physical and biological pretreatment.  
80 Biological methods are a good alternative to the physical and chemical methods as they are  
81 cost-effective and allow for lower energy use [8]. In nature, plant biomass is degraded by  
82 hydrolytic enzymes produced by microorganisms, including bacteria and fungi. Biologically  
83 stable and controllable microbial consortia with a high hydrolytic activity isolated from such  
84 environments, seem to be more valuable and effective than individually strains [9].

85         Many studies have shown that hydrolytic microbial consortia are very often isolated  
86 from different natural environments. Wongwilaiwalin et al. [10] developed stable  
87 thermophilic, lignocellulose-degrading microbial consortium (MC3F) from sugarcane bagasse  
88 compost, which can degrade up to 75% of rice straw, 70% of corn stover, and 60% bagasse in  
89 7 days. Haruta et al. [11] obtained a consortium (MC1) from composting materials (sugarcane  
90 dregs, chicken feces, dried straw, pig feces, and cattle feces). These stable community  
91 degraded 60% of rice straw, 88% of cotton, 70 % of corn stalk and 79% of filter paper. The  
92 biodiversity and varying hydrolytic efficiency of bacterial consortia isolated from different  
93 environments indicates the importance of the initial inoculum composition and its effect on  
94 the entire biogas production process.

95         Additionally, natural consortia are able to survive under a wide range of  
96 environmental conditions. Nowadays, remains a challenge to recognize and optimize  
97 degradation of maize silage by natural mesophilic bacterial consortia. Natural consortia are  
98 very diverse, both in terms of microbial biodiversity and cellulolytic activity [12]. Thus, the

99 selection, adaptation, stabilization and characterization of the natural consortia may play a key  
100 role in improving the degradation of the substrate and create an efficient way leading to the  
101 enhancement of biogas production during anaerobic digestion.

102 Although a number of studies have addressed to hydrolytic microbial consortia used  
103 for enhancing the mesophilic anaerobic digestion of maize silage, only few have focused on  
104 the actual changes in hydrolytic activity and biodiversity of microorganisms during the  
105 selection and adaptation processes. .

106 The purpose of this study was to evaluate the influence of the source of microbial  
107 community on the selection and stabilization of hydrolytic consortia designated for utilization  
108 of maize silage. Additionally, the effect of bioaugmentation of a stable methanogenic  
109 community with the adapted hydrolytic consortia on biogas production from maize silage was  
110 investigated.

## 111 **2. Materials and Methods**

### 112 **2.1. Source of microorganisms and substrate**

113 Hydrolytic microbial consortia were isolated from: (i) two mixed hydrolyzers of an  
114 agricultural biogas plant located in Miedzyrzec Podlaski (Poland), where maize silage is used  
115 as a substrate, (ii) cattle slurry from farms in Trzebieszow Pierwszy (Poland) and (iii) raw  
116 sewage sludge from the wastewater treatment plant "Czajka" in Warsaw (Poland).

117 Methanogenic consortium for anaerobic digestion was obtained from the fermenter  
118 tank of an anaerobic digester from the biogas plant in Miedzyrzec Podlaski (Poland).

119 Maize silage obtained from a farm in Mikanow (Poland) was homogenized in a  
120 blender, mixed with low-mineral water (Eden Springs, Poland) and used as a substrate for the  
121 selection of hydrolytic consortia and analysis of anaerobic digestion process.

### 122 **2.2. Experimental set-up for the selection of hydrolytic microbial consortia**

123 The selection of hydrolytic microbial consortia was carried out in 500 mL bottles . These lab-  
124 scale hydrolyzers were filled with 0.5% (v/v) of total solids (TS) of the aforementioned  
125 samples, 3% (v/v) of TS maize silage. Mineral water was added up to the final volume of 400  
126 mL. The selection process consisted of a series of 10 passages. Hydrolysis of maize silage in  
127 each passage lasted for 72 hours and was carried out at 30 °C. Samples for the estimation of  
128 hydrolytic activity were taken at the end of each passage. Samples for microbial community  
129 analysis were taken at the end of the passages: 1, 3, 6 and 10 and stored at -20 °C until DNA  
130 extraction.

### 131 **2.3. Estimation of the hydrolytic activity**

132 Semi-quantitative analysis of the hydrolytic activity, was determined by the modified method  
133 by Teather and Wood [13] using Congo-Red Dye as an indicator of hydrolytic (cellulolytic  
134 activity) of microorganisms. Supernatants from the cultures (8000 rpm, 10 min), obtained  
135 after each passage, were injected into metal cylinders placed on CMC-Congo Red agar plates  
136 (containing 1% Congo Red Dye) and incubated for 96 hours at 30 °C. A clear zone around a  
137 metal cylinder indicated the hydrolytic activity of the tested consortium.

138 The hydrolytic activity of the consortia after each passage was determined based on  
139 the assessment of the amount of reducing sugars (equivalent of glucose) generated during the  
140 enzymatic hydrolysis of insoluble cellulose (from maize silage). Reducing sugars  
141 concentration was estimated spectrophotometrically, by measuring the absorbance at 540 nm  
142 after the addition of 3 mL of 3,5-dinitrosalicylic acid (DNS) reagent to 1 mL of the  
143 centrifuged cultures [14].

### 144 **2.4. Hydrolysis of maize silage**

145 Laboratory-scale degradation of maize silage by the adapted ABH, CS and WTP  
146 consortia was carried out in 1 L bottles GL 45 (Schott Duran, Germany). The reaction mixture  
147 containing 3% TS maize silage was inoculated with 10% (v/v) of the selected consortia. The

148 pH was adjusted to 7.2 using sodium bicarbonate. The hydrolysis was carried for 120 hours at  
149 30 °C. Physical and chemical analyses were performed at the beginning of the experiment and  
150 every 24 hours until 120 hours. The following parameters were assessed for each sample:  
151 soluble chemical oxygen demand (sCOD), volatile fatty acids (VFAs) concentration and the  
152 total reducing sugar (glucose) released due to the hydrolytic activity of the consortia.

### 153 **2.5. Batch assay of the anaerobic digestion**

154 The effect of bioaugmentation of anaerobic digestion by the adapted hydrolytic consortia was  
155 investigated in laboratory-scale anaerobic batch experiments, which were performed in  
156 reactors consisting of 1 L glass bottles GL 45 (Schott Duran, Germany) connected with  
157 Dreschel-type scrubbers. To each reactor, a 1 L Tedlar gas bag (Sigma, Germany) was  
158 attached to collect biogas. The bioreactors were filled with the liquid phase from the  
159 fermenter tank of an anaerobic digester containing the methanogenic consortium inoculate  
160 [18 g volatile solids per liter ( $\text{g}_{\text{vs}} \text{L}^{-1}$ )], maize silage ( $9.6 \text{ g}_{\text{vs}} \text{L}^{-1}$ ) and supplemented with 100  
161 mL of the adapted hydrolytic consortia. Low-mineral water was added up to the final volume  
162 of 900 mL. The pH in each bioreactor was adjusted to 7.2 using sodium carbonate. Anaerobic  
163 batch assays were run at 37 °C for 21 days without refeeding. Physical and chemical analyses  
164 were carried out at the beginning of the experiment and after 7, 14 and 21 days. The  
165 experiment was performed in triplicate.

### 166 **2.6. Analytical methods**

167 To monitor the hydrolysis of maize silage and the anaerobic digestion process, the following  
168 parameters were determined: sCOD, VFAs concentration, the total reducing sugar (glucose)  
169 concentration and volume of the biogas produced. The VFAs concentration and sCOD were  
170 determined using Nanocolor® kits (Machery-Nagel GmbH, Germany). The total  
171 concentration of reducing sugar was determined by the method developed by Miller (1959).

172 The volume of the produced biogas was monitored by Milligascounter MGC-1 (Ritter,  
173 Germany).

## 174 **2.7. DNA extraction and PCR amplification**

175 Total DNA from the selected consortium was isolated using the method described by Dziewit  
176 et al. [15]. Briefly, the samples were centrifuged (8000 rpm, 4 °C, 15 min), pellet was  
177 resuspended in lysis buffer [100 mM Tris-HCl (pH 8.0), 100 mM sodium EDTA (pH 8.0),  
178 100 mM sodium phosphate (pH 8.0), 1.5 M NaCl, 1% (w/v) CTAB] and the cells were  
179 disrupted in a 5-step bead-beating protocol, supported by freezing and thawing procedure.  
180 Final DNA purification from protein, humic substances, etc., was carried by cesium chloride  
181 density gradient ultracentrifugation. The concentration and quality of the purified DNA was  
182 estimated by means of the NanoDrop 2000 instrument (NanoDrop Technologies) and gel  
183 electrophoresis.

184 The whole community DNA was used as a template for amplification of bacterial  
185 hypervariable V3–V4 regions of the 16S rDNA with the primers S-D-Bact-0341-b-S-17/S-D-  
186 Bact-0785-a-A-21, described by Klindworth et al. [16]. The reaction mixture (50 µL)  
187 contained 100 ng of the template DNA, primers and 0.02 U of Phusion High-Fidelity DNA  
188 Polymerase (Thermo Scientific). Bacterial 16S rDNA fragments were PCR amplified in a  
189 thermocycler (Biorad) with 20 cycles. PCR conditions were as follows: initial denaturation (5  
190 min at 96 °C), cycles consisting of denaturation (30 s at 96 °C), annealing (50 s at 58 °C),  
191 extension (25 s at 72 °C), and a final extension step (5 min at 72 °C). The PCR products were  
192 analyzed by horizontal gel electrophoresis (2% agarose with ethidium bromide in 1x TAE)  
193 and then purified with Agencourt AMPure XP beads (Beckman Coulter).

## 194 **2.8. Sequencing library preparation and amplicon sequencing**

195 To prepare the libraries for sequencing, approximately 250 ng of amplified DNA (pooled  
196 from the PCR replicates) was used with the Illumina TruSeq DNA Sample Preparation Kit

197 according to the manufacturer's protocol, except that the final library amplification step was  
198 omitted. Libraries were verified using the 2100 Bioanalyzer (Agilent) High-Sensitivity DNA  
199 Assay and KAPA Library Quantification Kits (Illumina).

200 Amplicon DNA sequencing was performed using the Illumina MiSeq Platform (MiSeq  
201 Illumina Kit V3) with a 300 bp read length. Computational analyses were performed in  
202 similar manner as described by Nelson et al. [17], using a local computing environment with  
203 the Quantitative Insights in Microbial Ecology (QIIME, v1.9.0) pipeline [18]. Briefly, raw  
204 sequences were processed with the Cutadapt software enabling trimming of the nucleotides  
205 corresponding to the sequence of adapters and primers used for PCR amplification and library  
206 preparation. In next step, the sequences were merged and combined into a single fastq file, in  
207 order to ensure an even treatment and comparison for QIIME analyses. This resulted in the  
208 generation of 2.4 mln sequences with the mean length of 422 nucleotides. Chimera detection  
209 was performed using usearch61 [19] with subsequent filtering from sequences. Operational  
210 taxonomic units (OTU) were *de novo* assigned with uclust [20], clustered at 97% similarity  
211 against the SILVA version 111 reference OTU alignment [21]. A representative sequence for  
212 each OTU was selected and then the taxonomic assignment was made using the RDP  
213 Classifier v2.2 [22]. Additional filtering for sequence errors was performed with  
214 filter\_otus\_from\_otu\_table.py script by removing OTUs appearing in fewer than 3 samples  
215 and represented by less than 0.0005% of the total sequences.

216 Taxonomic structures were prepared based on OTU tables specific for bacterial  
217 amplicons, with a family level default. Sequences that were not assigned at the family level  
218 were named in accordance with the lowest possible taxonomy. A principle coordinates  
219 analysis (PCoA) plot was constructed to visualize the dissimilarity of samples at different  
220 stages of selection.

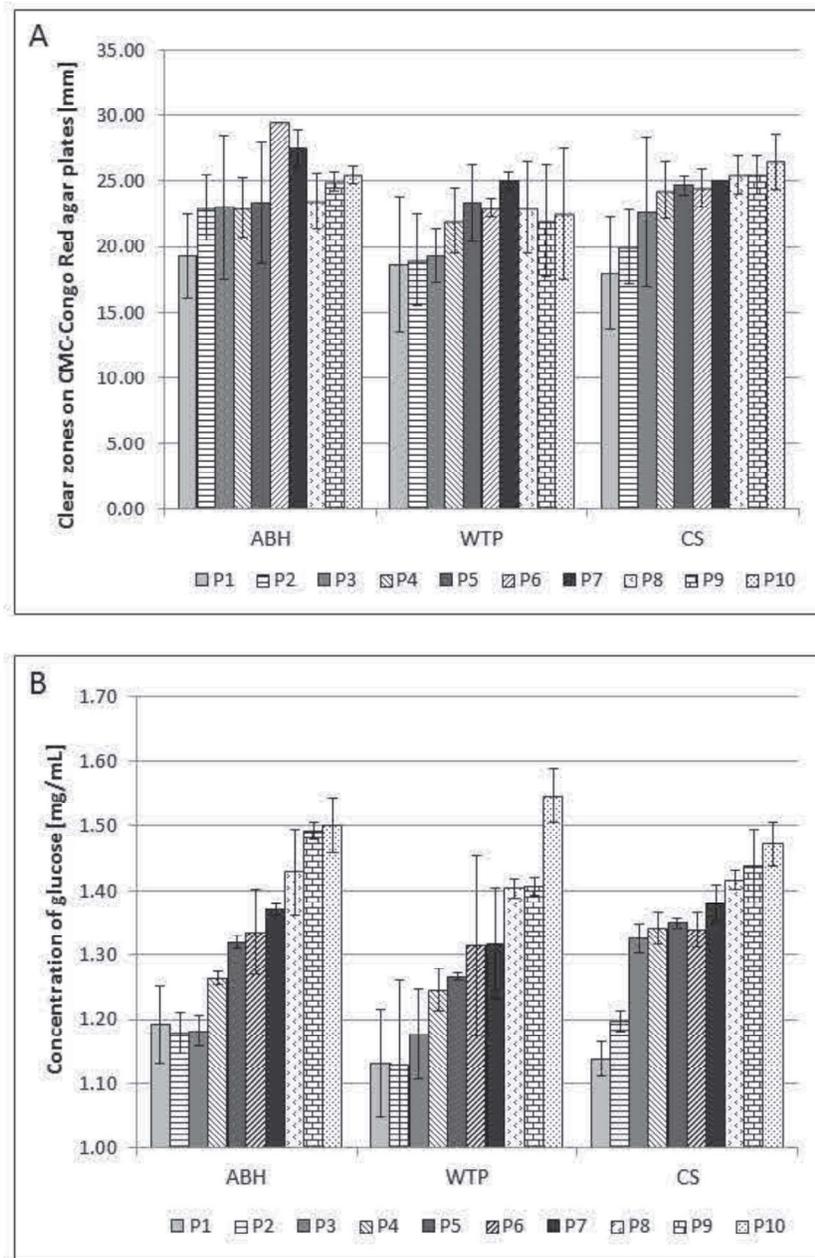
221 Raw sequences of 16S rDNA amplicons obtained in this study (15 libraries) were  
222 deposited in the SRA (NCBI) database under Bioproject accession number PRJNA350818.

### 223 **3. Results and discussion**

224 Hydrolytic microbial consortia were obtained after successive subcultivations of various  
225 environmental sources of microorganisms: (i) an effluent from a hydrolyzer tank from an  
226 agricultural biogas plant (ABH), (ii) cattle slurry (CS) and (iii) raw sewage sludge from a  
227 wastewater treatment plant (WTP) on medium containing maize silage. Selection and  
228 adaptation of the hydrolytic consortia was monitored during a series of 10 passages carried  
229 out every 72 hours at 30 °C on a fresh portion of maize silage medium. The performed  
230 experiments were aimed to find out: (i) the effect of the source of microorganisms on the  
231 hydrolytic activity of the selected consortia, (ii) biodiversity changes within these consortia  
232 and (iii) the effect of the selected consortia on degradation and anaerobic digestion of maize  
233 silage.

#### 234 **3.1. The effect of the source of microorganisms on the hydrolytic activity of the adapted** 235 **consortia**

236 To determine the changes in the hydrolytic activity of the analyzed consortia during each step  
237 of adaptation (each passage), basic physiological tests on the CMC-Congo Red medium agar  
238 plates were performed. After 96 hours of cultivation, the level of cellulolytic (hydrolytic)  
239 activity of studied the consortia was semi-quantitatively assessed by measuring the diameter  
240 of the produced clear zones (Fig. 1A).



241

242 **Fig. 1. Hydrolytic activity of the consortia during the selection process.** Analysis of the  
 243 changes: clear zones diameter on CMC-Congo Red agar plates (A) and concentrations of the  
 244 released glucose (B).

245 The initial diameter of the clear zones after first passage (P1) was 18-19 mm for all  
 246 consortia. The size of the clear zones has increased and reached the maximum diameter of

247 29.5 mm, 26.5 mm and 25.0 mm for ABH (after P6), CS (after P10) and WTP (after P7),  
248 respectively. These results indicate that all the selected consortia had hydrolytic (cellulolytic)  
249 activity and it was higher than that of the initial consortium after adaptation for used substrate.  
250 Literature data on the Congo red clearing zone assay, describes the results only for pure  
251 strains of bacteria. The results obtained in this study indicated that the level of hydrolytic  
252 activity of the analyzed consortia, corresponds to that described in the literature as a high for  
253 the pure strains. For example, Gupta et al. [23] obtained 28-50 mm clear zones for  
254 cellulolytic bacteria isolated from guts of termite, caterpillar, bookworm and snail, and Liang  
255 [24] – 20-30 mm clear zones for organic-rich soil isolates. Our earlier studies on hydrolytic  
256 strains (belonging to the following genera: *Bacillus*, *Ochrobactrum*, *Providencia*), which  
257 produced clear zones reaching from 15 to 44 mm in diameter. These strains were isolated  
258 from a hydrolyzer tank from an agricultural biogas plant, cattle slurry and manure and were  
259 dedicated for degradation of maize silage [25].

260 As previously stated, the diameter of the hydrolyzing zone produced by bacteria on  
261 CMC-Congo Red plates it is only semi-quantitative method for assessing the hydrolytic  
262 activity of bacteria and it may not accurately reflect their actual hydrolytic activity. For this  
263 reason the hydrolytic activity of the selected consortium was evaluated by analyzing the  
264 changes in the concentration of glucose released during maize silage degradation. Cleavage of  
265 the  $\beta$ -1, 4-glycosidic bonds by microbial enzymes leads to the hydrolysis of cellulose,  
266 resulting in the release of glucose or oligosaccharides. The amount of reducing sugars  
267 produced during the degradation of maize silage indicates the pretreatment effectiveness  
268 [26,27]. For the studied consortia, the initial concentrations of glucose in the first passage of  
269 all cultures were similar (1.13-1.19 g/L). During the selection process, the concentration of  
270 glucose gradually increased, reaching the highest value of 1.50 mg/mL, 1.58 mg/mL and 1.47  
271 mg/mL in the passage 10 for ABH, WTP and CS, respectively (Fig. 1B). The increase was  
272 equivalent to the release of 26% (ABH), 37% (WTP) and 29% (CS) more glucose molecules

273 compared to first passage and indicates a higher hydrolytic activity of the selected consortia.  
274 Additionally, the fastest increase in the concentration of glucose was observed for CS (1.34  
275 g/L after the third passage (P3)). CS had a higher increase at the beginning, which means it  
276 reached its peak reducing sugar yield earlier than the other two consortia. This trend was also  
277 observed in the clearing zone assay and thus suggested that cattle manure can be a good  
278 source of microorganisms for fast-acting and stable hydrolytic consortia.

279 Moreover, another aspect of the source of hydrolytic microorganisms are the nutrients  
280 it contains. The micronutrients contained in the source can enhance the metabolism of  
281 microorganisms and hydrolytic activity, and consequently, biogas yield [28,29]. However, the  
282 concentrations of micronutrients in different sources of microorganisms were rarely  
283 mentioned. In the case of using maize silage as a substrate, the concentration of nitrogen  
284 could be low with simultaneous excess of carbon, what may result in lower biogas production  
285 [30]. When cattle manures is used as source of microorganisms, extra nitrogen, present in the  
286 initial sample, is provided to meet the needs of the hydrolytic consortium. However, after the  
287 first passage, cattle slurry no longer constitutes a source of nutrients, what may have caused  
288 further decrease in the biodiversity of the consortium.

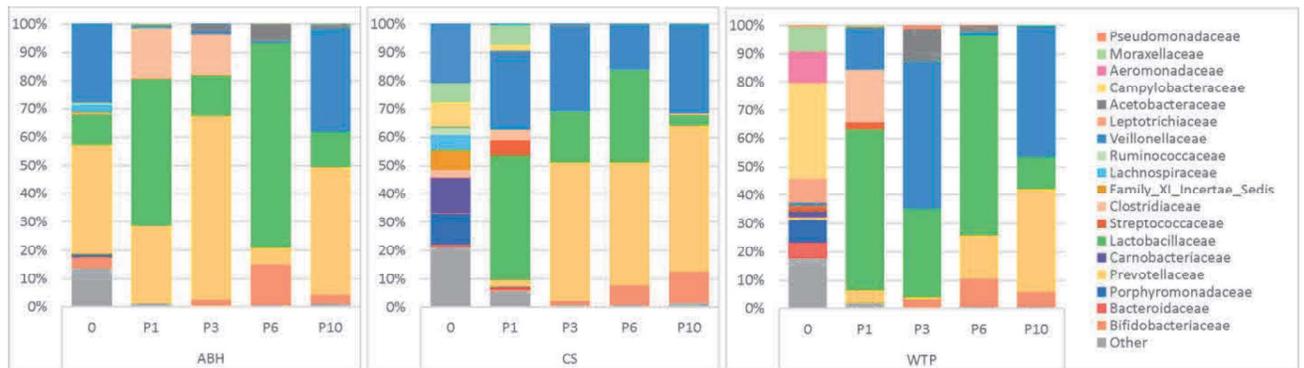
289 The results of CMC-Congo Red agar plates assay as well as the changes in  
290 concentrations of glucose released indicate that hydrolytic activity increased during  
291 experiments for all consortia and suggest the selection of specialized bacteria and adaptation  
292 for enhanced degradation of maize silage.

### 293 **3.2. The effect of the source of inoculum on the diversity changes during the adaptation** 294 **of the hydrolytic consortia**

295 Biodiversity of the microbial consortia was analyzed based on high throughput gene  
296 sequencing amplicons of hypervariable fragment V3-V4 of bacterial 16S rDNA. In the  
297 studied samples, 3 to 8 bacterial phyla constituting at least 1% of whole microbial community

298 were detected. The most abundant phylum was *Firmicutes* with the average count 60%  
 299 (ranging from 6% to 93%) followed by *Bacteroidetes* with 24% (ranging from 1% to 64%) of  
 300 total microbial sequences. Members of the *Firmicutes* and *Bacteroides* phyla play the most  
 301 important role in the hydrolysis of the plant biomass and in the secondary fermentation [31].

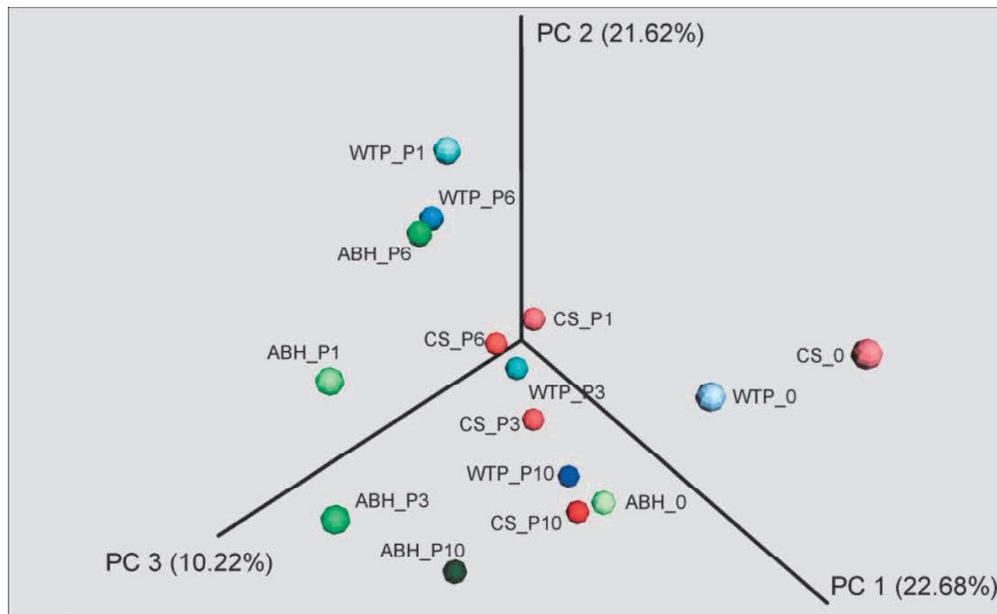
302 Considering the microbial structure at family level, the results clearly shows the  
 303 adaptation of the microbial communities (Fig.2).



304 **Fig. 2. Bacterial community structure dynamics.** The bar chart shows the relative  
 305 abundance of bacterial families with abundance > 5% in at least one variant. Inoculum  
 306 communities were denoted with 0 while the numbers 1, 3, 6, 10 represent the subsequent  
 307 passages as described in the Materials and Methods section. ABH – agricultural biogas  
 308 hydrolyzer, CS – cattle slurry, WTP – wastewater treatment plant.

310 The number of families (with >1% abundance) present in the inoculum samples were  
 311 reduced from 17 (CS), 12 (WTP) and 10 (ABH) to 4-5 families in each sample in the last  
 312 passage. For both ABH and WTP samples, a decrease in the dominating families (in the  
 313 percentage content of the families dominating in the initial sample) was already seen after the  
 314 first passage. For the remaining consortium CS, the reduction to 4-5 families occurred at  
 315 passage 3. This quick alteration of the microbial community structure can indicate a fast  
 316 response of the microorganisms to the changes in conditions and selection of specialized best-  
 317 adapted bacteria. Confirmation of the adaptation of microbial communities was presented by

318 Principal Coordinates Analysis (PCoA) of the Bray-Curtis dissimilarity indices (Fig. 3).  
319 These data indicate diversity differences between the communities and also within the  
320 consortia after successive passages. The original sources of ABH, CS and WTP were  
321 significantly different, while the consortia adapted after 10 passages have a very similar  
322 structure (Fig. 3).



323  
324 **Fig. 3. Principal Coordinates Analysis (PCoA Bray-Curtis) of differences in bacterial**  
325 **diversity observed during the selection of microbial communities.** Spheres representing  
326 each sample were colored according to their origin as follows: agricultural biogas hydrolyzer,  
327 ABH – green, cattle slurry, CS – red, wastewater treatment plant, WTP – blue. The intensity  
328 of colors increases with the passage number.

### 329 3.2.1. Agricultural biogas hydrolyzer (ABH) community

330 The inoculum originating from the agricultural biogas hydrolyzer was dominated by  
331 the representatives of *Prevotellaceae* (39%), *Veillonellaceae* (28%) and *Lactobacillaceae*  
332 (11%) families. These groups of bacteria are characterized by a strong hydrolyzing activity  
333 towards polysaccharide compounds resulting in high production of volatile fatty acids (VFA)

334 [32,33]. Since the ABH inoculum was obtained from a full-scale biogas plant utilizing maize  
335 silage as a substrate, the initial microbial community was already adapted to maize  
336 degradation and was characterized by a strong hydrolyzing activity. During the cultivation  
337 experiments, at the next two analyzed time-points, we observed shifts between the dominating  
338 bacteria *Lactobacillaceae* and *Prevotellaceae* with the relative abundance of 52% and 27% at  
339 passage 1 and 15% and 64% at passage 3, respectively. Additionally, the family  
340 *Clostridiaceae* emerged from below 1% to 18% (ABH1) and 14% (ABH3). Members of this  
341 family are well-known for their high cellulolytic activity [34] and thus release of simpler  
342 sugars from polysaccharides, which eventually leads boosted the growth of *Lactobacillaceae*  
343 (72%) and *Bifidobacteriaceae* (15%) in our study. Bacteria belonging to these families are  
344 known to produce lactic acid as one of the main products of carbohydrate fermentation  
345 degradation [35,36]. Interestingly at the end of the experiments, the abundance of dominant  
346 bacterial families, *Prevotellaceae* (45%), *Veillonellaceae* (36%) and *Lactobacillaceae* (13%),  
347 almost reflected that of inoculum but with reduced importance of low abundant families.

### 348 3.2.2. Cattle slurry (CS) community

349 Most of the sequences identified within the CS inoculum were affiliated with non-cellulolytic  
350 *Pseudomonadaceae* (21%), *Carnobacteriaceae* (12%), *Campylobacteriaceae* (8%) and  
351 *Moraxellaceae* (7%), as well as microorganisms capable of fermentation of carbohydrates:  
352 *Porphyromonadaceae* (12%), *Lachnospiraceae* (5%) and probably Family XI Incertae Sedis  
353 (7%) [37,38,39]. After the first passage a drastic (1100-fold) increase in the abundance of  
354 *Lactobacillaceae* to the level of 44% of all the bacterial sequences was observed. Second  
355 most abundant family became *Veillonellaceae* (27%) with over 90-fold greater coverage in  
356 microbial structure. Moreover, all of the previously dominating bacteria (except  
357 *Moraxellaceae*) were diminished to the level below 0.5%. This drastic shift indicates very fast  
358 changes in bacterial community structure in response to substrate pressure. In the passage 3,

359 hemicellulose- and pectin-degrading *Prevotellaceae* (49%) gain dominance, which is in  
360 accordance with the results of a previously showed in a high-concentrate diet experiment [33].  
361 As a result of the improved cellulose degradation, an increase in abundance of fast growing  
362 carbohydrate fermenters, which often produce lactic acid, namely *Lactobacillaceae* (33%)  
363 and *Bifidobacteriaceae* (7%) was observed after the passage 6. Similarly to the ABH  
364 community, after the passage 10 the microbial community structure was again dominated by  
365 *Prevotellaceae* (51%) and *Veillonellaceae* (31%), but instead of lactobacilli,  
366 *Bifidobacteriaceae* (11%) remained the third most abundant family. Moreover, in the case of  
367 the CS consortium thereafter the passage 3 we observed the most stable microbial structure  
368 (calculated as the smallest difference between the dominant families in the P3-P10 passages)  
369 of all studied consortia. This observation can explain more stable performance of CS  
370 community in the CMC-Congo clearing zones measurement and glucose concentration.

### 371 3.2.3. Wastewater treatment plant (WTP) community

372 The inoculum originating from the wastewater treatment plant was composed of many non-  
373 cellulolytic families such as *Campylobacteraceae* (34%), *Aeromonadaceae* (11%),  
374 *Moraxellaceae* (9%), and *Leptotrichiaceae* (9%). The families which could be affiliated to  
375 polysaccharide and VFA utilization included *Porphyromonadaceae* (8%) and *Bacteroidaceae*  
376 (5%) [38]. In the selection experiment after substrate change to maize silage, we observed the  
377 dominance of *Lactobacillaceae* (57%) with approximately 440-fold increase compared to the  
378 initial community. The change in the bacterial community structure was similar to that  
379 detected in the previously described variants. However, the second and the third most  
380 abundant families became *Clostridiaceae* (19%) and *Veillonellaceae* (15%) which can explain  
381 differences in CMC-Congo clearing zones and glucose concentration tests. In the next  
382 analyzed step, the selection of bacteria also occurred in a slightly different way. After passage  
383 3, members of *Veillonellaceae* (52%), *Lactobacillaceae* (31%) and *Acetobacteraceae* (12%)

384 dominated in the community. Members of the genus *Acetobacter* primarily contribute to  
385 acetate production [40].  
386 After passage 6, members of *Lactobacillaceae* again outcompeted other bacteria with the  
387 relative abundance of 71%, but at the end of experiment their number was reduced to 12%.  
388 Passage 10 was dominated by *Veillonellaceae* (46%) and *Prevotellaceae* (36%).

389 In the above experiments, adaptation of three communities towards consortia highly  
390 specialized in degradation of maize silage was observed. Although the community structure of  
391 the initial consortia was very different, from the third passage the dominance of bacteria  
392 belonging to six families: *Lactobacillaceae*, *Prevotellaceae*, *Veillonellaceae*, *Clostridiaceae*,  
393 *Bifidobacteriaceae* and *Acetobacteraceae* was observed. This could be an indicator of  
394 selection and qualitative stabilization of the bacterial communities but, on the other hand, the  
395 relative abundance of the above-mentioned bacterial families varied between the passages,  
396 excluding quantitative stability. In the adapted consortia, members of the families  
397 *Lactobacillaceae*, *Prevotellaceae*, *Veillonellaceae* were the most important as they were  
398 characterized by the highest average count (Fig. 2). In all the variants, adaptation the selection  
399 process began with an increase in the relative abundance of fast growing *Lactobacillaceae*,  
400 specialized in oligosaccharide degradation and production of short chain fatty acids (SCFA),  
401 mainly lactic acid [35]. Enrichment of the consortia with members of this family was  
402 previously observed in studies where agricultural materials were used for anaerobic digestion  
403 [41,42]. Wirth et al. [43] obtained interesting results which reported that indigenous  
404 microorganisms of maize silage include representatives of the genera *Lactobacillus* and  
405 *Acetobacter*.

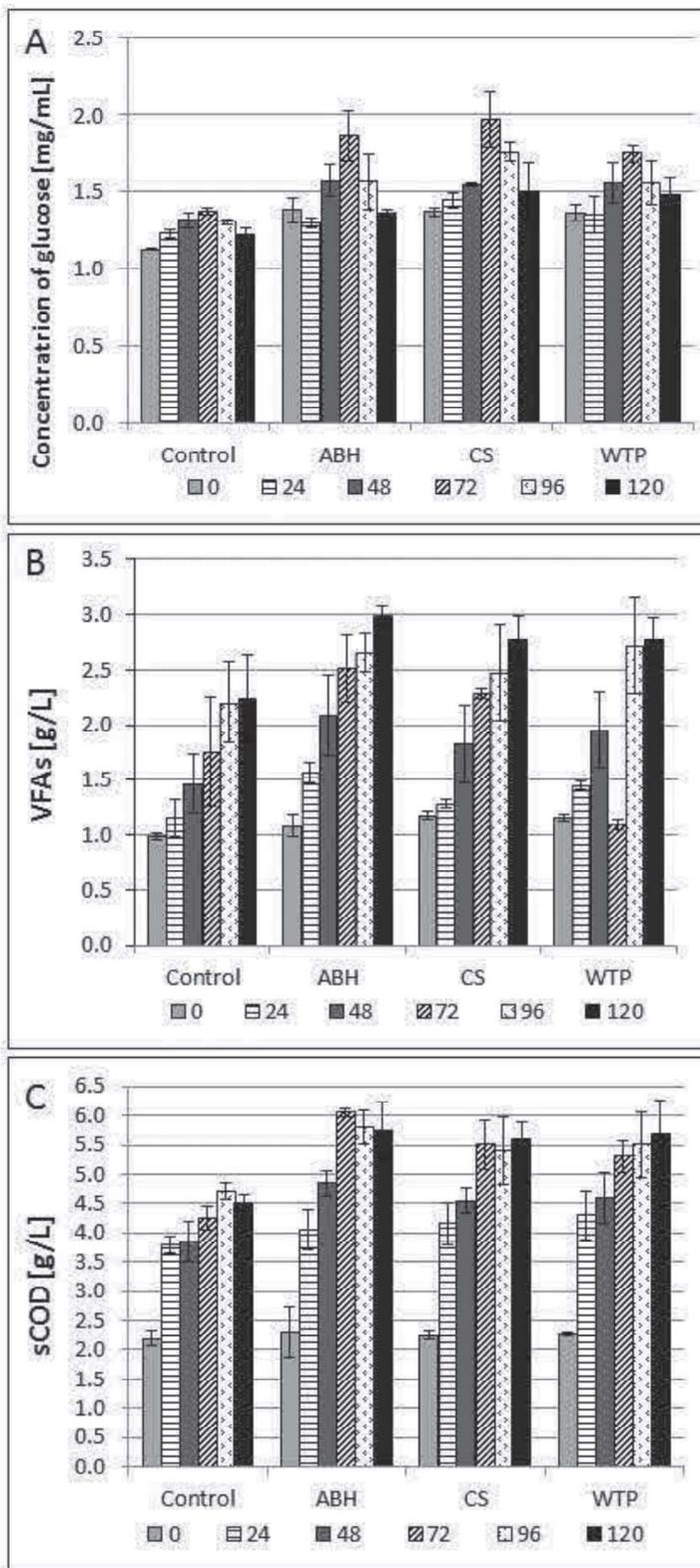
406 Our results of selection process of the analyzed consortia was driven by substrate input  
407 rather than the composition of the initial inoculum, which differed with the origin of the  
408 sample. After cultivation on maize silage, the multiple families present in sources samples

409 (even very low abundant <0.1%) in the subsequent passages emerged 3-6 families involved in  
410 maize silage degradation. De Francisci et al. [44] also observed that selection process caused  
411 changes in the bacterial population by substrate input but not the sample origin. In turn,  
412 Porsch et al. [45] indicated that only the initial enrichment step significantly influence the  
413 adaptation and changes of microbial community structure of wheat straw. The subsequent  
414 passages did not affect the structure and activity of the community.

### 415 **3.3. Functional analysis of the adapted consortia**

#### 416 *3.3.1 Hydrolysis of maize silage*

417 To analyze the hydrolytic potential of the adapted consortia, 120-hour anaerobic batch  
418 cultures on maize silage were performed. The control variant consisted of maize silage/low  
419 mineral water medium, which was treated exactly as the culture variants, except for the  
420 inoculation with hydrolytic consortia. The efficiency of maize silage hydrolysis was  
421 expressed as a function of concentration of the produced (released) glucose and VFAs, as well  
422 as the level of sCOD (Fig 4.).



423

424

**Fig. 4. Solubilization of maize silage by the adopted hydrolytic consortia.** Changes in the

425

concentration of: glucose (A) and VFAs (B), as well as the level of sCOD (C) were analyzed.

426 The concentration of glucose increased from 1.12 g/L to 1.37 g/L in the control variant,  
427 from 1.38 g/L to 1.85 g/L for ABH, from 1.37 g/L to 1.97 g/L for CS and from 1.36 g/L to  
428 1.75 g/L for WTP after 72 hours. These were the highest glucose concentrations obtained  
429 during the experiment. Longer hydrolysis resulted in a decrease in glucose concentration in all  
430 the cultures, what is probably caused by the consumption of sugars by microorganisms (Fig.  
431 4). The concentration of VFAs was increased in all variants during 120 hours. In the control  
432 increased concentrations of VFAs from 0.99 g/L to 2.24 g/L were observed. in the variants  
433 where adopted consortia were added the concentrations of VFAs increased from 1.08 g/L to  
434 2.99 g/L for ABH, from 1.17 g/L to 2.78 g/L for CS and from 1.15 g/L to 2.77 g/L for WTP. (  
435 The obtained results showed an increase in the amount of reducing sugars (glucose) and  
436 VFAs formed/released during the degradation of maize silage. The production of volatile fatty  
437 acids may also play an important role in enhancing the degradation of maize silage. Zhang  
438 and co-workers [29] suggested that mild acids can loosen the structure of maize silage leading  
439 to an improved overall rate of hydrolysis due to increased accessibility of the substrate for  
440 hydrolytic enzymes which would further benefit production of biogas.

441 The initial value of sCOD in all the cultures was similar (2.2-2.3 g/L) and it increased  
442 throughout the experiment. The highest level of sCOD was observed after 72 hours for ABH  
443 (6.05 g/L), and 120 hours for CS and WTP (5.6 g/L and 5.7 g/L, respectively). In the control,  
444 the highest level of sCOD was obtained after 96 hours (only 4.7 g/L) and then it decreased.  
445 Faster increase in sCOD maybe an indicator of the accelerated maize silage degradation.

446 The observed increase in sCOD as well as glucose and VFAs concentrations probably  
447 resulted from the metabolic activity of the indigenous microbiota of maize silage. Ensiling is a  
448 well-known technology for preserving lignocellulosic material. Microbial silage starters  
449 (lactic acid bacteria) are very often added during the process in order to ensure rapid  
450 acidification or the formation of specific metabolites which inhibit the growth of other  
451 organisms, which may cause spoilage of plant matter [46,47].

452 Cultivation of hydrolytic consortia in natural media has been previously described by  
453 many researches. In 2010, Guo et al. [48] obtained a lignocellulose-degrading composite  
454 microbial system (XDC-2) from soil amended with composted agricultural and animal waste.  
455 The concentration of reducing sugars obtained after the degradation of rice straw and corn  
456 stalk was 1.3 g/L and 2.4 g/L, respectively. Yuan et al. [49] showed that the VFAs  
457 concentration and sCOD increased rapidly during 4 days (120 hours) of pretreatment of corn  
458 stalk using the MC1 consortium, and their values differed depending on the initial  
459 concentration of the substrate.

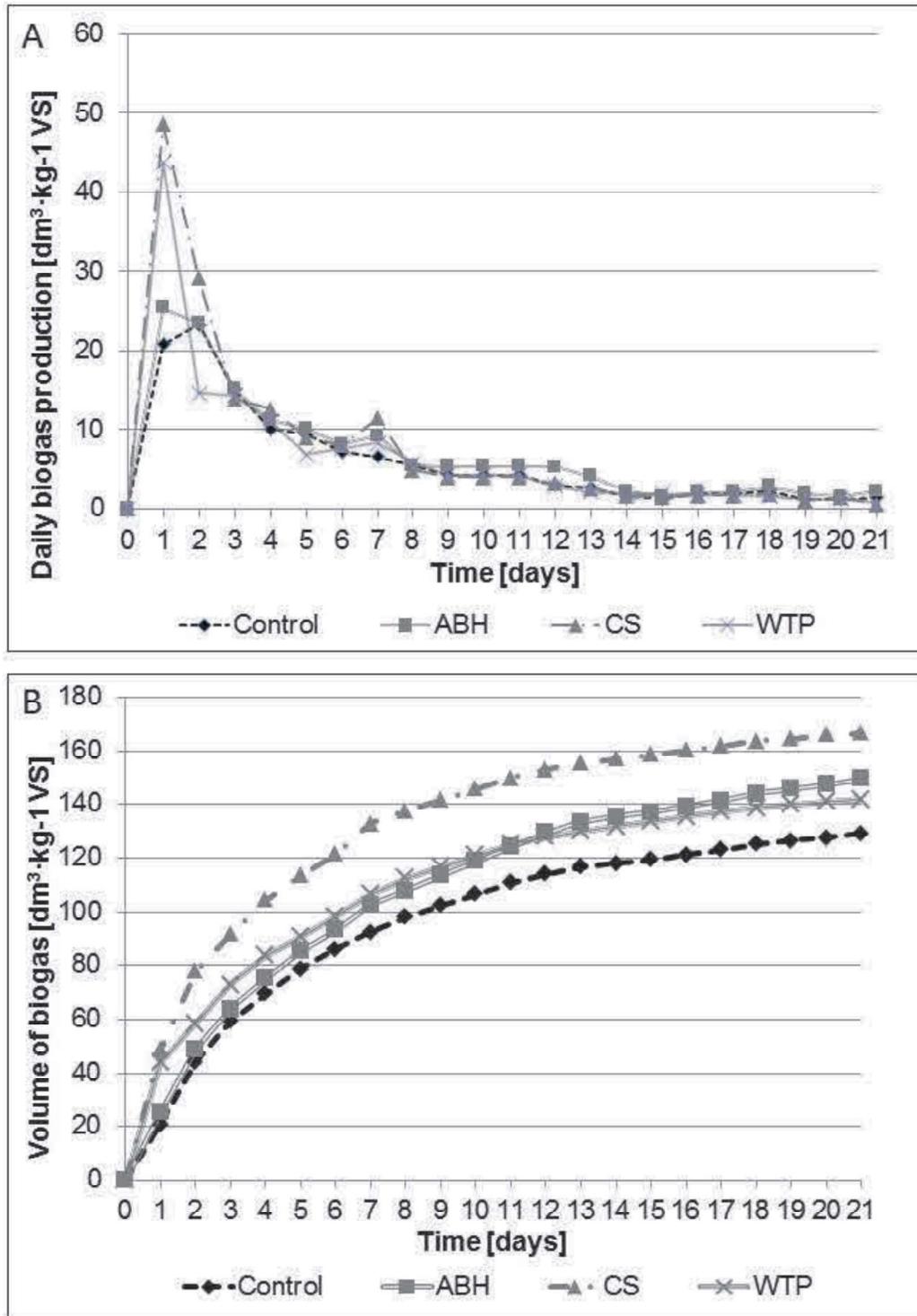
460 Our results also indicated an increase in VFAs and glucose concentrations, as well as  
461 the level of sCOD during hydrolysis. This was mainly due to the degradation of insoluble  
462 macro-molecular organic compounds of maize silage by hydrolytic activity of analyzed  
463 consortia. The intermediate products of hydrolysis, could probably be utilized by other groups  
464 of microorganisms during the next phase of anaerobic digestion.

### 465 *3.3.2. The influence of the adapted consortia on degradation and anaerobic digestion of* 466 *maize silage*

467 The selection process of microbial communities to degrade maize silage was confirmed both  
468 in experiments testing hydrolytic activity and bacterial community structure based on 16S  
469 rDNA survey. In the next step of our experiments we used the adapted consortia in order to  
470 verify if and how the hydrolytic ABH, CS and WTP consortia may affect the activity of  
471 methanogenic community of biogas plant fermenter tank and ultimately its efficiency of  
472 biogas production.

473 To determine the effect of augmentation of the anaerobic digestion communities by  
474 ABH, CS and WTP consortia on the efficiency of maize silage anaerobic digestion (biogas  
475 production), a batch cultures experiment was carried out. The analyzed hydrolytic consortia  
476 were added to the anaerobic digester only once at the beginning of the experiment. The liquid

477 phase from the fermenter tank of anaerobic digester from a biogas plant was used as a the  
478 source of methanogenic consortium. During 21 days simulation of maize silage anaerobic  
479 digestion process, VFAs concentration, sCOD and the daily biogas production were  
480 measured. The physical and chemical parameters affect the anaerobic digestion process. The  
481 first phase of simulation of anaerobic digestion was hydrolysis. According to the literature,  
482 hydrolysis does not take more than 5 days, so it was decided to determine VFAs, and sCOD  
483 only after 7 days, and at the end of entire process (21 days). The obtained results show that  
484 VFAs concentration and sCOD increased during the anaerobic digestion in all batch assays  
485 (Tab. 1). The concentration of VFAs increased from 5.88 g/L to 10.29 g/L, from 5.61 g/L to  
486 10.06 g/L, and from 6.12 g/L to 10.11 g/L , for the ABH, CS and WTP variants respectively),  
487 after 7 days. In the control variant VFAs concentration increased from 5.37 g/L to 9.33 g/L  
488 during the same time, and then decreased to 8.96 g/L after 21 days.. It was observed that  
489 VFAs concentrations in culture ABH, CS and WTP, remained at high level even after 21  
490 days, and amounted 10.37 g/L, 12.06 g/L and 10.71 g/L, respectively. The initial value of  
491 sCOD (18.43 – 18.80 g/L) was increased (to 22.50 g/L for ABH, 23.47 g/L for CS and 23.20  
492 g/L for WTP, after 7 days. After 21 days, the values of this parameter had increased to 24.93  
493 g/L for ABH, 25.90 g/L for CS and 26.10 g/L for WTP. In the control, sCOD was increased  
494 from 18.63 g/L to 20.83 g/L after 7 days and to 24.63 g/L after 21 days. Concentrations of  
495 VFAs were higher by 10%, 48%, 8% after 21 days for ABH, CS and WTP, respectively,  
496 compared to the control. The level of sCOD was higher by 4%, 6% and 9% after 21 days, for  
497 ABH, CS and WTP, respectively, than in the control. Our results suggest that  
498 bioaugmentation of maize silage by hydrolytic consortia contributes to an improvement in  
499 decomposition (liquefaction) of this substrate during anaerobic digestion. The analysis to the  
500 daily and cumulative biogas production (CBP) revealed that the hydrolytic consortia (ABH,  
501 CS and WTP) increased the efficiency of biogas production from maize silage (Fig. 5A and  
502 Fig. 5B).



503

504 Fig. 5. The efficiency of biogas production during anaerobic digestion of maize silage: A)

505 daily biogas production and B) cumulative biogas production.

506 CBP for anaerobic digestion of maize silage with the addition of hydrolytic  
507 consortium was 150 dm<sup>3</sup>/kg of VS and 166.5 dm<sup>3</sup>/kg of VS and 141.8 dm<sup>3</sup>/kg of VS for ABH,  
508 CS and WTP, respectively. The production of biogas in the experiment without  
509 bioaugmentation (control) was 128 dm<sup>3</sup>/kg of VS. The results showed that the high  
510 production of biogas was maintained for 7 days. After this time, in the variants with  
511 hydrolytic consortia, biogas production was higher by about 10%, 43% and 15% (for ABH,  
512 CS and WTP, respectively) than in the control variant. This was probably caused by the  
513 increased efficiency of maize silage hydrolysis related to the presence of the analyzed  
514 consortia during the entire anaerobic digestion process.

515 The obtained results indicate that biogas production increased by 16%, 29% and 10%  
516 after bioaugmentation of the methanogenic consortia with ABH, CS and WTP, respectively.

517 The results of physical and chemical analyses show that the accumulation of  
518 intermediate products (VFAs) and soluble substrate (as indicated by the increased level of  
519 sCOD) after hydrolysis facilitated by the hydrolytic consortia ABH, CS and WTP, may be  
520 beneficial for the anaerobic digestion process and it was correlated with the improved  
521 efficiency of biogas production (Fig. 5B). Moreover the addition of the adapted hydrolytic  
522 consortia to the anaerobic digestion process increased the activity of methanogenic  
523 consortium. Furthermore, effective hydrolysis means a short digestion time and this may  
524 increase the overall biogas production efficiency [50]. This could bring significant economic  
525 benefits for increasing the biogas production efficiency or treatment capacity of anaerobic  
526 digesters because of the shortened digestion time.

#### 527 **4. Conclusions**

528 In this study the effect of the source of microorganisms on the selection and adaptation of  
529 hydrolytic microorganisms was analyzed. The obtained results showed that subsequent  
530 passages of hydrolytic consortia using maize silage as substrate led to the selection of the

531 representatives of three families of bacteria: *Lactobacillaceae*, *Prevotellaceae* and  
532 *Veillonellaceae*, which dominate in the investigated communities after the adaptation process.  
533 This indicates that the substrate, not the community origin was the main driving force in the  
534 adaptation of hydrolytic consortia.

535         Following adaptation, hydrolytic capabilities of all three consortia have improved, as  
536 indicated by the increased concentration of the released glucose, VFAs, and the level of  
537 sCOD in the culture. Moreover, bioaugmentation of anaerobic digestion using the adapted  
538 hydrolytic consortia increased the efficiency of biogas production by up to 29%. This proves  
539 that subsequent passaging of hydrolytic consortia on an appropriate substrate, such as maize  
540 silage, prior to their application in biogas plant hydrolyzers, may facilitate their adaptation  
541 and increase their hydrolytic activity.

542         Future work should involve the selection and characterization of the key hydrolytic  
543 microorganisms found in the analyzed consortia, as well as investigation of the mechanism of  
544 their activity, which leads to the enhancement of biogas production during anaerobic  
545 digestion.

#### 546 **Author contributions**

547 KP: planned and performed the selection, hydrolysis and anaerobic digestion experiments, as  
548 well as most of the chemical analyses, DNA isolation and wrote the manuscript; AP: was  
549 involved in planning of the metagenomics approach, performed the deep sequencing and  
550 bioinformatics analysis, and was involved in writing of the manuscript; ASob and LL:  
551 designed and supervised the metagenomics and bioinformatics approaches; ASklo: is the head  
552 of a group, and was involved in consultation and article correction; LD: is the head of a  
553 project; planned and directed the studies and was involved in consultation and article  
554 preparation.

555

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559 **References**

- 560 [1] W. Parawira, M. Murto, J. S. Read, B. Mattiasson, Study of two-stage anaerobic  
561 digestion of solid potato waste using reactors under mesophilic and thermophilic  
562 conditions, *Environ. Technol.* 28 (2007) 1205-1216.
- 563 [2] C.A. O’Sullivan, P.C. Burrell, The effect of media changes on the rate of cellulose  
564 solubilisation by rumen and digester derived microbial communities, *Waste Manage.* 27  
565 (2007) 1808-1814.
- 566 [3] H.W. Yu, Z. Samani, A. Hanson, G. Smith, Energy recovery from grass using two-  
567 phase anaerobic digestion, *Waste Manage.* 22 (2002) 1-5.
- 568 [4] A. Schievano, A. Tenca, B. Scaglia, G. Merlino, A. Rizzi, D. Daffonchio, R. Oberti, F.  
569 Adani, Two-stage vs single-stage thermophilic anaerobic digestion: comparison of energy  
570 production and biodegradation efficiencies. *Environ. Sci. Technol.* 46 (2012) 8502–8510
- 571 [5] J. Lindner, S. Zielonka, H. Oechsner, A. Lemmer, Is the continuous two-stage  
572 anaerobic digestion process well suited for all substrates? *Bioresour. Technol.*, 200 (2015)  
573 470-476.
- 574 [6] B.K. Ahring, Status on science and application of thermophilic anaerobic digestion,  
575 *Water Sci. Tech.* 30 (12) (1994) 241-249.
- 576 [7] DBFZ (Deutsches Biomasseforschungszentrum gemeinnützige GmbH).  
577 Stromerzeugung aus Biomasse (Vorhaben IIa Biomasse). Zwischenbericht.  
578 Projektnummer DBFZ, Leipzig: 2015

- 579 [8] A.M. Mshandete, L. Björnsson, A. K. Kivaisi, M. S. T. Rubindamayugi, B.  
580 Mattiasson, Two-stage anaerobic digestion of aerobic pre-treated sisal leaf decortication  
581 residues: hydrolases activities and biogas production profile, *Afr J. Biochem. Res.* 2  
582 (2008) 211-218.
- 583 [9] T.R. Zuroff, S.B. Xiques, W.R. Curtis, Consortia-mediated bioprocessing of cellulose  
584 to ethanol with a symbiotic *Clostridium phytofermentans*/yeast co-culture, *Biotechnol.*  
585 *Biofuels* 6 (2013) 59
- 586 [10] S. Wongwilaiwalin, U. Rattanachomsri, T. Laothanachareon, L. Eurwilaichitr, Y.  
587 Igarashi, V. Champreda, Analysis of a thermophilic lignocellulose degrading microbial  
588 consortium and multi-species lignocellulolytic enzyme system, *Enzyme Microb. Technol.*  
589 47 (2010) 283-290.
- 590 [11] S. Haruta, Z. Cui, Z. Huang, M. Li, M. Ishii, Y. Igarashi, Construction of a stable  
591 microbial community with high cellulose-degradation ability, *Appl. Microbiol.*  
592 *Biotechnol.* 59 (2002) 529-534.
- 593 [12] T.R. Zuroff, W.R. Curtis, Developing symbiotic consortia for lignocellulosic biofuel  
594 production, *Appl. Microbiol. Biotechnol.* 93 (2012) 1423-1435.
- 595 [13] R.M. Teather, P.J. Wood, Use of Congo red-polysaccharide interactions in  
596 enumeration and characterization of cellulolytic bacteria from the bovine rumen. *Appl.*  
597 *Environ. Microb.* 43 (4) (1982) 777-780.
- 598 [14] G.L. Miller, Use of dinitrosalicylic acid reagent for determination of 589 reducing  
599 sugar, *Anal. Chem.* 31 (1959) 426.

600 [15] L. Dziewit, A. Pyzik, K. Romaniuk, A. Sobczak, P. Szczesny, L. Lipinski, D.  
601 Bartosik, L. Drewniak, Novel molecular markers for the detection of methanogens and  
602 phylogenetic analyses of methanogenic communities, *Front. Microbial.* 6 (2015).

603 [16] A. Klindworth, E. Pruesse, T. chweer, J. Peplies, C. Quast, M. Horn, F.O. Glöckner,  
604 Evaluation of general 16S ribosomal RNA gene PCR primers for classical and next-  
605 generation sequencing-based diversity studies, *Nucleic Acids Res.* (2012) doi:  
606 10.1093/nar/gks808

607 [17] M.C. Nelson, H.G. Morrison, J. Benjamino, S.L. Grim, J. Graf, Analysis,  
608 optimization and verification of Illumina-generated 16S rRNA gene amplicon surveys,  
609 *PloS one* 9 (4) (2014) e94249

610 [18] J.G. Caporaso, J. Kuczynski, J. Stombaugh, K. Bittinger, F.D. Bushman, E.K.  
611 Costello, N. Fierer, A. Gonzalez Pena, J.K. Goodrich, J.I. Gordon, G.A. Huttley, S.T.  
612 Kelley, D. Knights, J.E. Koenig, R.E. Ley, C.A. Lozupone, D. McDonald, B.D. Muegge,  
613 M. Pirrung, J. Reeder, J.R. Sevinsky, P.J. Turnbaugh, W.A. Walters, J. Widmann, T.  
614 Yatsunenko, J. Zaneveld, R. Knight, QIIME allows analysis of high-throughput  
615 community sequencing data, *Nature Methods* 7 (2010) 335-336.

616 [19] R.C. Edgar, B.J. Haas, J.C. Clemente, C. Quince, R. Knight, UCHIME improves  
617 sensitivity and speed of chimera detection, *Bioinformatics* 27 (16) (2011) 2194-2200

618 [20] R.C. Edgar, Search and clustering orders of magnitude faster than BLAST,  
619 *Bioinformatics* 26 (2010) 2460-2461.

620 [21] C. Quast, E. Pruesse, P. Yilmaz, J. Gerken, T. Schweer, P. Yarza, J. Peplies, F.O.  
621 Glöckner, The SILVA ribosomal RNA gene database project: improved data processing  
622 and web-based tools, *Nucl. Acids Res.* 41 (2013) D590-6.

- 623 [22] Q. Wang, G.M. Garrity, J.M. Tiedje, J.R. Cole, Naive Bayesian classifier for rapid  
624 assignment of rRNA sequences into the new bacterial taxonomy, *Appl. Environ. Microb.*  
625 73 (16) (2007) 5261-5267S.
- 626 [23] P. Gupta, K. Samant, A. Sahu, Isolation of cellulose degrading bacteria and  
627 determination of their cellulolytic potential. *Int. J. Microbiol. Res.* (2012) doi:  
628 10.1155/2012/578925
- 629 [24] Y.L. Liang, Z. Zhang, M. Wu, Y. Wu, J.X. Feng, Isolation, screening, and  
630 identification of cellulolytic bacteria from natural reserves in the subtropical region of  
631 China and optimization of cellulase production by *Paenibacillus terrae* ME27-1. *Biomed.*  
632 *Res. Int.* 13 (2014) doi: 10.1155/2014/512497.
- 633 [25] K. Poszytek, M. Ciekowska, A. Sklodowska, L. Drewniak, Microbial Consortium  
634 with High Cellulolytic Activity (MCHCA) for Enhanced Biogas Production, *Front.*  
635 *Microbiol.* (2016) 7:324 doi: 10.3389/fmicb.2016.00324.
- 636 [26] R. Kumar, C.E. Wyman, Effect of enzyme supplementation at moderate cellulase  
637 loadings on initial glucose and xylose release from corn stover solids pretreated by leading  
638 technologies, *Biotechnol. Bioeng.* 102 (2) (2008) 457–467.
- 639 [27] N. Mosier, C.E. Wyman, B.E. Dale, R. Elander, Y.Y. Lee, M. Holtzapple, M.  
640 Ladisch, Features of promising technologies for pretreatment of lignocellulosic biomass,  
641 *Bioresour. Technol.* 96 (2005) 673-686.
- 642 [28] H. Pobeheim, B. Munk, J. Johansson, G.M. Guebitz, Influence of trace elements on  
643 methane formation from a synthetic model substrate for maize silage, *Bioresour. Technol.*  
644 101 (2) (2010) 836-839.

645 [29] L. Zhang, Y.W. Lee, D. Jahng, Anaerobic co-digestion of food waste and piggery  
646 wastewater: focusing on the role of trace elements, *Bioresour. Technol.* 102 (8) (2011)  
647 5048-5059.

648 [30] R. Chandra, H. Takeuchi, T. Hasegawa, Methane production from lignocellulosic  
649 agricultural crop wastes: a review in context to second generation of biofuel production,  
650 *Renew. Sustain. Energy Rev.* 16 (3) (2012) 1462-1476.

651 [31] R. Wirth, E. Kovács, G. Maróti, Z. Bagi, G. Rákhely and K. L. Kovács,  
652 Characterization of a biogas-producing microbial community by short-read next  
653 generation DNA sequencing, *Biotechnol. Biofuels* (2012) 5:41 doi: 10.1186/1754-6834-5-  
654 41

655 [32] J. Purushe, D.E. Fouts, M. Morrison, B.A. White, R.I. Mackie, North American  
656 Consortium for Rumen Bacteria, P.M. Coutinho, B. Henrissat, K.E Nelson K.E  
657 Comparative genome analysis of *Prevotella ruminicola* and *Prevotella bryantii*: insights  
658 into their environmental niche, *Microb. Ecol.* 60 (4) (2010) 721-729.

659 [33] S.C. Fernando, H.T. Purvis, F.Z. Najar, L.O. Sukharnikov, C.R. Krehbiel, T.G.  
660 Nagaraja, B.A. Roe, U. DeSilva, Rumen microbial population dynamics during adaptation  
661 to a high-grain diet, *App. Environ. Microbiol.* 76 (22) (2010) 7482-7490.

662 [34] E. A. Bayer, J.P. Belaich, Y. Shoham, R. Lamed, The cellulosomes: multienzyme  
663 machines for degradation of plant cell wall polysaccharides. *Annu. Rev. Microbiol.* 58  
664 (2004) 521-554

665 [35] W.P. Hammes, C. Hertel, The genera *Lactobacillus* and *Carnobacterium*, in: M.  
666 Dworkin, S. Falkow, E. Rosenberg, K.H. Schleifer, E. Stackebrandt (Eds.), *Prokaryotes*,  
667 Springer US, 2006, pp. 320-403.

- 668 [36] K. Pokusaeva, G.F. Fitzgerald, D. van Sinderen, Carbohydrate metabolism in  
669 *Bifidobacteria*, Genes Nutr. 6 (3) (2011) 285-306.
- 670 [37] M. Cotta, R. Forster, The family Lachnospiraceae, including the genera *Butyrivibrio*,  
671 *Lachnospira* and *Roseburia*, in: Dworkin, S. Falkow, E. Rosenberg, K.H. Schleifer, E.  
672 Stackebrandt (Eds.), Prokaryotes, Springer US, 2006, pp. 1002-1021.
- 673 [38] L. Regueiro, M. Carballa, J.M. Lema, Outlining microbial community dynamics  
674 during temperature drop and subsequent recovery period in anaerobic co-digestion  
675 systems. Res. J. Biotechnol. 192 (2014) 179-186.
- 676 [39] S. Chen, H. Cheng, K.N. Wyckoff, Q. He, Linkages of *Firmicutes* and *Bacteroidetes*  
677 populations to methanogenic process performance. J. I. Microbiol. Biot. 43 (6) (2016)  
678 771-781.
- 679 [40] H. Sträuber, R. Lucas, S. Kleinsteuher, Metabolic and microbial community  
680 dynamics during the anaerobic digestion of maize silage in a two-phase process. App.  
681 Microbiol. Biot. 100 (1) (2016) 479-491.
- 682 [41] P. Raspor, D. Goranovič, Biotechnological application of acetic acid bacteria. Crit.  
683 Rev. Biotechnol. 28 (2008) 101-124.
- 684 [42] R. Victor, S. Shajin, R.M. Roshni, S.R. Asha, Augmentative invention of biogas from  
685 the agronomic wastes using facultative anaerobic bacterial strain. Int. J. Curr. Microbiol.  
686 App. Sci. 3 (4) (2014) 556-564.
- 687 [43] R. Wirth, G. Lakatos, G. Maróti, Z. Bagi, J. Minárovics, K. Nagy, É. Kondorosi, G.  
688 Rákhely, and K. L. Kovács, Exploitation of algal-bacterial associations in a two-stage  
689 biohydrogen and biogas generation process. Biotechnol Biofuels. (2015); 8: 59 doi:  
690 10.1186/s13068-015-0243-x.

- 691 [44] D. De Francisci, P. G. Kougias, L. Treu, S. Campanaro, I. Angelidaki, Microbial  
692 diversity and dynamicity of biogas reactors due to radical changes of feedstock  
693 composition, *Bioresource Technol.* 176 (2015) 56-64.
- 694 [45] K. Porsch, B. Wirth, E. M. Tóth, F. Schattenberg and M. Nikolausz, Characterization  
695 of wheat straw-degrading anaerobic alkali-tolerant mixed cultures from soda lake  
696 sediments by molecular and cultivation techniques. *Microb. Biotechnol.* 8(5) (2015) 801-  
697 814.
- 698 [46] Z.G. Weinberg and R.E. Muck, New trends and opportunities in the development and  
699 use of inoculants for silage, *FEMS Microbiol. Rev.* 19 (1996) 53-68
- 700 [47] M. Holzer, E. Mayrhuber, H. Danner R. Braun, The role of *Lactobacillus buchneri* in  
701 forage preservation, *Trends Biotechnol.* 21 (6) (2003) 282-287.
- 702 [48] P. Guo, K. Mochidzuki, D. Zhang, H. Wang, D. Zheng, X. Wang, Z. Cui, Effects of  
703 different pretreatment strategies on corn stalk acidogenic fermentation using a microbial  
704 consortium, *Bioresour. Technol.* 102 (2011) 7526-7531.
- 705 [49] X. Yuan, B. Wen, X. Ma, W. Zhu W., X. Wang, Sh. Chen, Z. Cui, Enhancing the  
706 anaerobic digestion of lignocellulose of municipal solid waste using a microbial  
707 pretreatment method. *Bioresour. Technol.* 154 (2014) 1-9.
- 708 [50] M. Zheng, X. Li, L. Li, X. Yang, Y. He, Enhancing anaerobic biogasification of  
709 corn stover through wet state NaOH pretreatment, *Bioresour. Technol.* 100 (2009) 5140-  
710 5145.

711 **Table legends**

712 **Table 1. The physical and chemical characteristics of digester during anaerobic**  
713 **digestion.**

	VFAs			sCOD		
	[g/L]			[g/L]		
	0 days	7 days	21 days	0 days	7 days	21 days
<b>Control</b>	5.37±0.82	9.33±0.43	8.96±0.71	18.63±0.35	20.83±0.31	24.63±0.5
<b>ABH</b>	5.88±0.19	10.29±0.74	10.37±0.53	18.43±0.55	22.50±0.7	24.93±0.86
<b>CS</b>	5.61±0.13	10.06±0.13	12.06±0.05	18.80±0.21	23.47±0.26	25.90±0.35
<b>WTP</b>	6.12±0.11	10.11±0.46	10.71±0.58	18.47±0.53	23.20±0.21	26.10±0.5

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